

PRINCIPLES OF SELECTING NOZZLES FOR OIL REFINERY

REACTORS

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ABSTRACT	KEYWORDS
The article examines the issues of new ways to increase the efficiency of technological processes and improve the internal devices of reactors, the location of nozzles on the surface of the plate, gas flow rates, the cross-section of the nozzle with a flat diffuser.	Burner, diffuser, nozzle, flow velocity, turbulence, combustion zone.

Introduction

At present, reactors of petrochemical plants use distribution plates with a large number of tubular nozzles, the design of which varies. Modern requirements for the quality of oil refining products, in particular for the content of harmful impurities (for example, sulfur), force us to look for new ways to increase the efficiency of technological processes and improve the internal devices of reactors containing a catalyst layer. Reactors use open-type nozzles, while other manufacturers close the outlet section of the nozzle branch pipe with a flat divider, installing it at a distance of 0.1-0.25 percent of the branch pipe diameter.

In these nozzles, the liquid flow is supplied to the diffuser, highly dispersed distribution, having a perforation degree of 2-3%, uniform arrangement of nozzles on the surface of the plate. The corresponding gas flow rates in the nozzle pipes are provided by the assignment of the perforation degree of the plate and are 2.4-4.15 m/s for the specified flow range.

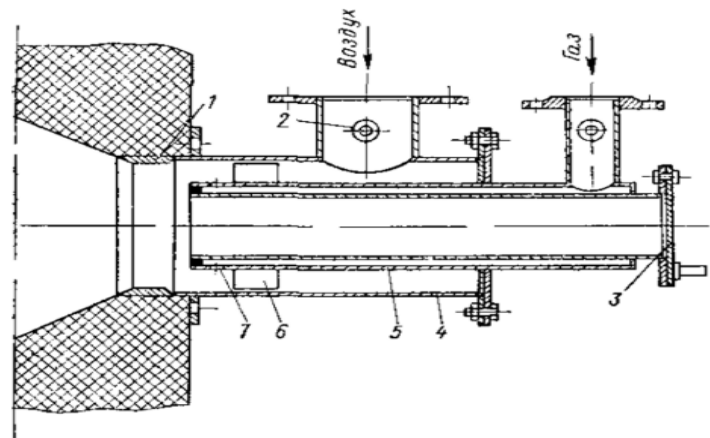


Figure 1. Open type injectors

Numerous experiments have shown that for this type of flows in the zone between the distribution plate and the catalyst bed, the influence of the similarity criteria of the Froude and Euler numbers is practically insignificant. The structure of the gas flow is determined mainly by the Reynolds number, i.e. the influence of viscous forces, therefore, when determining the parameters of the experimental setup, we proceeded from the requirement of equality of the Reynolds numbers for flows in natural (in reactors) and experimental conditions, which would ensure the identity of the flow pattern in the studied zones.

The Reynolds number for the flow zone under consideration is appropriate to determine by the parameters of the nozzle branch pipes: internal diameter of 40 mm and flow velocity through the nozzle V m/sec. Let us dwell on the choice of the type of flow as the working medium and compare the corresponding indicators of kinematic viscosity and. Average value for the working flow in reactors: $0.9875 \cdot 10^{-6}$ m²/sec, Corresponding values for air and water, m²/sec; water $1.0 \cdot 10^{-6}$. air $18.09 \cdot 10^{-6}$ Comparing the kinematic viscosities of the working flow in the reactor, water and air, we see a practical coincidence of their values for the working medium and water. It follows that the Reynolds numbers determined for the reactor zone and the experimental setup will coincide under the following conditions:

- identity of the geometry of the nozzles and the flow zone under study;
- the working fluid that forms the flow in the experimental setup;
- equality of flow rates through nozzles in full-scale and experimental setups.

Since the flow occurs at high pressure and temperature, the implementation of these conditions during the experimental work requires separate consideration. When implementing these conditions in the experimental setup, the flow structures, their dynamics and other indicators obtained during the experimental work will be identical to the processes occurring in reactors under the operating conditions of their operation. In this case, there is no need to create high pressures and maintain high temperatures.

2. Materials and research methods

The geometric appearance of the experimental setup is determined from the following conditions. Due to the symmetry of the placement of the nozzles over the area of the plate, each of them has its own zone of influence, limited on the sides by six zones from neighboring nozzles with similar parameters, inside which the flow structure is formed. Interaction with neighboring flows from other nozzles occurs along the common boundaries of the zone. To obtain a flow pattern in the zone of action of the nozzle, taking into account the influence of neighboring zones, a "cut" of the working zone is carried out in depth from the plate to the catalyst layer with three nozzles located in one line, while the choice of the direction of this line in the plane of the plate is of no importance due to the symmetry of the arrangement of the nozzles.

3. Research results

The experimental work was carried out as part of a certified reference pouring stand intended for testing measuring instruments for the needs of heat engineering. The stand is equipped with measuring and automation instruments for creating and maintaining water flow rates and speeds with the required accuracy.

The experimental setup has a removable transparent panel on the top and a transverse metal insert on which three nozzles with replaceable diffusers are mounted. Each nozzle has a pipeline for feeding colored liquid into the nozzle branch pipe to visualize the flow pattern. The colored liquid is fed from a separate container and under pressure. Water was used as the working medium, as defined above. The setup is designed to operate under pressure up to 0.1 MPa.

From a wide variety of nozzle divider options, five of the most functionally and technologically promising ones in terms of manufacturing and installation were selected.

For each variant of the diffuser, the flow rate in the nozzle branch pipe was varied during the tests, m/e: 2.4; 3.3; 4.15.

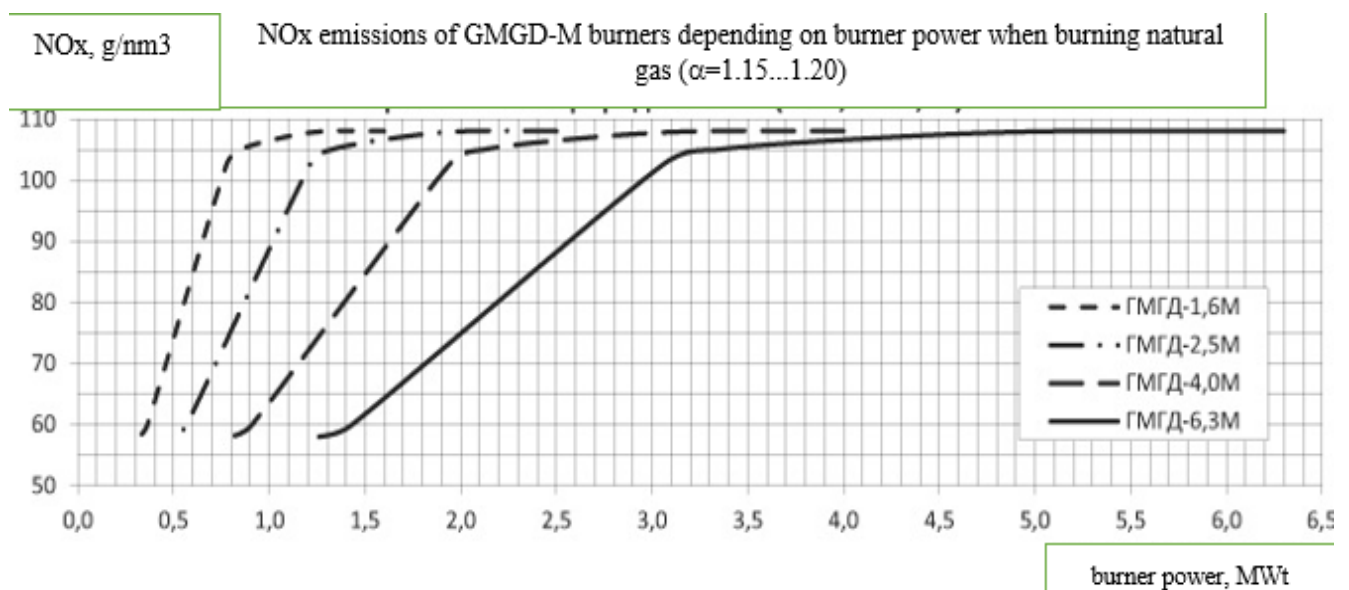
The flow structures were recorded for 300 seconds by a portable video camera and, after computer processing, were converted into computer video films and frame-by-frame file structures with a frequency of 50 frames/sec.

It should be noted that the flow rates through the nozzles were formed and maintained by the stand systems stationary during the entire time of pouring a specific variant, whereas for all variants of diffusers and flow modes in the studied zone, non-stationary flow patterns with different linear scales of turbulence and parameters of vortex structures were formed, which corresponds to Reynolds numbers of $2.5 \cdot 10^5$.

4. Analysis of research results

Based on the experiment, it was established that the greatest uniformity of the flow structure or the least turbulence is provided by nozzles with diffusers of option No. 3.

This diffuser has a perforated disk with a perforation rate of 15-27%, diameter $d = 1.500$ (d is the internal diameter of the nozzle), installed at a distance h_d from the branch pipe cut. The flow pattern is characterized by uniform expansion downstream with a weak turbulent structure, i.e. with weak velocity disturbances in the cross section of the jet, which can be taken as the required flow structure. An increase in the flow velocity leads to an increase in the scale of turbulence, but to acceptable values, i.e. extensive vortex structures with reverse flows are not formed.



Based on the research, it has been experimentally established and when comparing the structure of the flows formed by all the considered variants of the nozzles, it is evident that the greatest uniformity of the flow structure or the least turbulence is provided by the nozzle with the diffusers of variant No. 3.

5. Conclusions and recommendations

Considering the obvious advantages in the formation of the flow as a whole behind the reactor distribution plate, as well as the technological efficiency of manufacturing this version of the diffuser, the gas-oil burner GMGD-4.0M is recommended for use in the design of the nozzle as part of the distribution plate as a whole.

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